

An H₃O-Alunite Method for Production of Smelter Grade Alumina from an Ammonium Alum Solution after High-Pressure Acid Leaching of Coal Fly Ash

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Abstract

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Precipitation of H₃O-alunite from an ammonium alum solution using boehmite as a seed was studied. The ammonium alum solution was obtained after high-pressure leaching of mullite-type coal fly ash (CFA) with a mixture of 7.5 M H₂SO₄ + 40 % NH₄HSO₄ at 200 °C. Fe(III) was extracted from the ammonium alum solution by ion exchange sorption using the Purolite S957 resin. Effects of temperature (70–90 °C), seed boehmite (100–400 g/L), ammonium alum (60–240 g/L), and precipitation duration (2–8 h) on the Al precipitation degree were evaluated. Calcination of the precipitate at 300–950 °C to obtain alumina powder was studied next. Concentration of impurities, specific surface area, phase composition, morphology, and the average particle size distribution of alumina powders were investigated. The results show that smelter grade aluminium (SGA) can be obtained at optimized parameters of precipitation and calcination

Keywords: Coal fly ash, Ammonium bisulphate method, H₃O-alunite precipitation, Smelter grade alumina, Waste utilization.

1. Introduction

The rapid growth of the aluminium industry requires a search for new cheap sources of aluminium. Such raw materials can be industrial waste: a bauxite residue (“red mud”) [1], coal gangue [2], or salt aluminium dross [3]. Nonetheless, the most promising raw material is coal fly ash (CFA) from coal-fired power plants because its annual generation in the world is more than 1000 Mt [4]. This waste occupies vast territories and leads to pollution of soils and rivers [5]. A search for new recycling methods will reduce the negative impact of this waste and will help to obtain, in addition to alumina, many valuable products such as iron-based alloys [6], lithium (Li) [7], rare-earth elements [8], coagulants [9], silicon-potassium mineral fertilizer [10], CaSiO₃ and silica gel [11], unburned carbon [12], Al–Si master alloy [13], Ni and V [14], zeolites [15], cenospheres for construction materials [16].

The Al₂O₃ content of CFA reaches 25 to 40 %, and silicon oxide (SiO₂) concentration is 35 to 65 %. This Al/Si ratio makes it difficult to employ traditional alkaline Bayer and sintering methods in order to produce SGA because some of the sodium hydroxide will be wasted due to the interaction with SiO₂ during the leaching process [17]. Therefore, acidic methods are being developed that involve hydrochloric acid (HCl) [18], sulphuric acid (H₂SO₄) [19], or nitric acid (HNO₃) [20]. The most promising approach is to use a mixture of sulphuric acid and ammonium bisulphate (NH₄HSO₄) [21]. This technique allows the separation of Al from the solution by

precipitation of ammonium alum $[(\text{NH}_4)\text{Al}(\text{SO}_4)_2 \cdot 12\text{H}_2\text{O}]$ after filtration of the leaching solution with a temperature decrease from 90 to 25 °C [22].

There are many ways to obtain aluminium oxide from ammonium alum: direct roasting at 900–1300 °C [23] or precipitation of pseudoboehmite (AlOOH) by neutralization with ammonia under atmospheric [24] or hydrothermal conditions [25] with subsequent calcination at 1100 °C [26]. Additives (sodium dodecylbenzene sulphonate) can be employed to increase the average particle size from 20.1 to 31.3 μm in the pseudoboehmite powder [27]. An increase in the particle size of boehmite was observed when a significant amount of ammonium alum was added and the neutralization process was undertaken for a period of 18 h [28]. The coprecipitation method with the addition of ammonium hydrogen carbonate (NH_4HCO_3) has also been studied [29]. During precipitation, ammonium aluminium carbonate hydroxide $[\text{NH}_4\text{Al}(\text{OH})_2\text{CO}_3]$ has been obtained, and after calcination at 900 °C, a powder mixture containing $\gamma\text{-Al}_2\text{O}_3$ and $\alpha\text{-Al}_2\text{O}_3$ has been produced [30]. Recent studies have shown the possibility of precipitation of aluminium from ammonium alum solution by neutralization method using gibbsite as a seed [31]. However, the temperature of calcination from gibbsite for smelter grade alumina production is 1200 °C [32]. This is 300 °C higher than the temperature of boehmite calcination [33], so the emphasis in this research was on the use of boehmite as a seed.

In the present paper, for the first time, a method is proposed for the precipitation of the H_3O -alunite salt on the surface of seed boehmite without additional reagents. As a result, it is possible to produce smelter grade alumina from CFA by the ammonium bisulphate method in accordance with Russia, China, and India state standards.

2. Materials and Methods

2.1 Materials and Reagents

CFA was collected from Reftinskaya GRES (Sverdlovsk Oblast, Russia; 57.10°N, 61.70°E): the largest coal-fired power plant in Russia. The raw CFA consisted of 62.43 wt.% of SiO_2 , 24.66 wt.% of Al_2O_3 , and 3.32 wt.% of Fe_2O_3 . Phase composition of CFA was as follows: mullite ($3\text{Al}_2\text{O}_3 \cdot 2\text{SiO}_2$), quartz (SiO_2), and magnetite (Fe_3O_4) [34]. Seed aluminium hydroxide was obtained from Urals Aluminium Smelter (Sverdlovsk Oblast, Russia; 56.36°N, 61.96°E). Analytical-grade sulphuric acid (H_2SO_4 , 93%) and ammonium bisulphate (NH_4HSO_4) were purchased from SigmaTek (Moscow, Russia).

2.2 Experiments

To conduct experiments with boehmite powder, seed aluminium hydroxide $[\text{Al}(\text{OH})_3]$ was calcined in a PM-1 muffle furnace (Plavka.Pro, Russia) at 350 °C for 3 h. The yield after calcining was 74–76 % of the initial mass of gibbsite. In addition to the change in phase composition, SSA (Specific Surface Area) of the powder enlarged from 0.5 to 213.6 m^2/g .

In precipitation tests, the temperature of the ammonium alum solution (50 mL) was 70, 80, or 90 °C; seed boehmite concentration was 100, 200, or 400 g/L, ammonium alum concentration 60, 120, or 240 g/L; and precipitation time 2, 4, or 8 h. The slurry obtained after the precipitation was filtered, and the powder was washed with hot water and dried at 105 °C for 4 h. Next, the powder was weighed and analysed, and the Al precipitation degree was calculated using the following equations.

$$M_{\text{H}_3\text{O-alunite}} = (M_p \times C_s/100) \times 6.16 \quad (1)$$

4. Conclusions

A bisulphate method for CFA recycling for SGA production was investigated in this work. The main conclusions are as follows:

The effects of solution temperature, seed boehmite amount, ammonium alum concentration, and of precipitation duration on Al precipitation were examined by the ANN method. The use of optimized parameters [$T = 90\text{ }^{\circ}\text{C}$, seed AlOOH at 400 g/L , $(\text{NH}_4)\text{Al}(\text{SO}_4)_2 \cdot 12\text{H}_2\text{O}$ at 120 g/L , and $\tau = 8\text{ h}$] led to an Al precipitation extent of 88 %.

The phase transformation, the sulphur content, and BET values of boehmite with H_3O -alunite were determined after calcination at $300\text{--}950\text{ }^{\circ}\text{C}$. The resulting SGA powder contained approximately 20 % $\kappa\text{-Al}_2\text{O}_3$ and 80 % $\gamma\text{-Al}_2\text{O}_3$ at $900\text{--}950\text{ }^{\circ}\text{C}$. The sulphur content was 0.34 wt.% and SSA was $51.7\text{ m}^2/\text{g}$ at the calcination temperature of $950\text{ }^{\circ}\text{C}$. A method for sulphur removal from boehmite with H_3O -alunite by NH_4OH treatment is proposed. The sulphur content of SGA was reduced to 0.06 wt.%.

The chemical composition and the particle size distribution of the SGA powder derived from CFA were also analysed. It was demonstrated that in terms of chemical composition and SSA, the SGA powder meets the state standards of Russia, China, and India.

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